ICR2008 Monterey USA
Puzzling over Pressure with John Dealy
Shaw Receives Distinguished Service Award
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The Society of Rheology invites you to participate in the XVth International Congress on Rheology (ICR), which will take place in Monterey, California USA from 3-8 August 2008. The Congress convenes every four years and brings together the world’s leading rheologists to present the latest advances and developments in our field.

The 2008 Congress will take place at the Monterey Conference Center in Monterey, California. The host hotels are the Portola Plaza Hotel and the Monterey Marriott, with views of the famous Old Fisherman’s Wharf and walking distance to Cannery Row and Monterey Bay Aquarium. Situated on the Monterey Bay, the largest marine sanctuary in the United States, the town of Monterey is an international vacation destination with incredible restaurants, exciting recreational facilities, and fascinating points of interest.

The Congress technical program has been designed to highlight significant topics in contemporary rheology. The opening plenary lecture on Monday morning will be presented by Paul Callaghan from the School of Chemical and Physical Sciences at Victoria University of Wellington, New Zealand. Prof. Callaghan’s talk, “From molecules to mechanics: nuclear magnetic resonance and rheological insight,” will give an overview of his efforts to combine the nanoscale probe capability of NMR with rheology to obtain information about soft matter. The Congress will include a closing plenary lecture on Friday afternoon by Fred MacKintosh from the Department of Physics and Astronomy of Vrije Universiteit, the Netherlands. Prof.

Organizing Committee (Local Arrangements)

Gerald Fuller (co-chair), Stanford University
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Andrew M. Kraynik, Sandia National Laboratories
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MacKintosh, an internationally respected researcher on soft matter physics, will speak on “Non-equilibrium mechanics of active gels and living cells.” New to ICR2008, Prof. MacKintosh’s lecture will be followed by a reception/lunch that will bring the Congress to a close early Friday afternoon. The Congress week will be filled with fourteen keynote lectures (including the SOR’s Bingham lecture), contributed oral presentations organized into sixteen mini-symposia, a poster session, and social activities including a Wednesday afternoon excursion, a beach party, and a banquet. Attendees are encouraged to come to Monterey Sunday 3 August or earlier and to stay through the closing Friday afternoon reception.

Two short courses will be offered on the weekend before the Congress, 2-3 August 2008. A two-day short course on Suspension Rheology will be given by Jan Mewis and Norman Wagner. A one-day short course on Surfactant Rheology - Self-Assembly and Microstructure Dynamics will run on Sunday 3 August, taught by Pat Spicer and Srinivasa Raghavan. Those interested in both topics may take one day of the Suspension course followed by the Surfactant course. Details on the short courses are available in a separate article in this Bulletin (page 8) and on the web at www.rheology.org/ICR2008/ShortCourse/ShortCourse.htm.

The highlight of the ICR social calendar will be the Wednesday afternoon excursion, which is included for full delegates and for registered accompanying persons. There will be a choice of seven excursions, one for every taste. There are two choices for winery tour, the Carmel Valley Wine Tour and the Steinbeck Country Wine Tour. Both tours involve visits to multiple wineries and ample time for sampling. For those who prefer the sea, there is a Big Sur Coastline Tour. This tour takes participants by bus down the renowned Big Sur coast, to enjoy dramatic land and sea vistas along the way. Breathtaking scenery includes ancient redwood groves and a wide variety of California wildlife, including the ever-popular sea otter. If you prefer to be on the water, there is the Monterey Marine Sanctuary Whale Watching Tour. A short walk from the Convention Center takes us to Fisherman’s Warf, the starting point for a cruise exploring some of the marine sanctuary’s 276 miles of shoreline and 5,322 square miles of ocean. Whales in the bay during the summer months include Blue Whales, Sperm Whales, and Fin Whales, and Monterey Bay is abundant with all kinds of life from sea otters and sea lions to dolphins and pelicans.

For the more active conferees there are three excursions to choose from, the Kayak Tour, the Bike Tour, and Golf at Poppy Hills. The docent-guided Kayak Tour will

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**Program for Full Delegates**

- **Sunday Afternoon Arrival**
- **Sunday Vendor Displays Open**
- **Sunday Evening Reception**

**Monday Opening Plenary:**
- **Paul Callaghan (Rheo-NMR)**
- **Monday Sessions**
- **Monday Evening Reception**

**Tuesday Sessions**
- **Wednesday Morning Sessions**
- **Wednesday Afternoon Excursion,** choice of:
  - Carmel Valley Wine Tour
  - Steinbeck Country Wine Tour
  - Big Sur Coastline Tour
  - Monterey Marine Sanctuary Whale Watching Tour
  - Kayak Tour
  - Bike Tour
  - Golf at Poppy Hills
- **Wednesday Night Beach Party**
  - 7:00 pm Pirate's Cove

**Thursday Sessions**
- **Thursday Evening Reception and Banquet**

**Friday Morning Sessions**
- **Friday late Morning Plenary:**
  - **Fred MacKintosh (Gels)**
- **Friday Closing Ceremonies**
- **Friday Reception/Lunch**

**Saturday Morning Departure**

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**Technical Program Co-Chairs**
L. Gary Leal, U. California Santa Barbara
Ralph Colby, Pennsylvania State Univ.
explore the Monterey Bay up close, and participants will learn about the ecology of the bay, the history of the area, and about the biology and habits of the varied marine life. The Bike Tour explores the Monterey Bay coastline on a specialized 24-speed hybrid bike (helmet provided). Finally, for . . . well, you know who you are, there’s Golf at Poppy Hills. Poppy Hills, located in Pebble Beach, California and designed by Robert Trent Jones, II, is a challenging, par-72 venue that weaves through the Del Monte Forest and plays host to several renowned tournaments, including the AT&T Pebble Beach National Pro-Am.

Monterey can be accessed conveniently with direct flights into Monterey Peninsula Airport from San Francisco, Los Angeles, and Salt Lake City. Ground transportation using express shuttles and buses can also be obtained from the San Francisco, Oakland, and San Jose Airports. A regularly scheduled service is operated by Monterey Airbus. The travel time by car from the San Francisco airport is approximately 2.5 hours. For more information on transportation and tours, visit the Monterey County Convention and Visitors Bureau (montereyinfo.org). For information about U.S. visa policy and procedures, visit UnitedStatesVisas.gov or Travel.State.gov.

Registration for full delegates and student delegates includes access to all technical sessions and the vendor display, the program and abstract booklets, the CD of Congress Proceedings, selected social events, and coffee breaks. An extensive Accompanying Persons Program has been organized. Registration fees are $650 USD (before 15 April)/ $750 USD (after 15 April) for delegates, $200/$250 USD for student delegates, and $350 USD for accompanying persons (no deadline).

Student members of The Society of Rheology are invited to apply for travel grants to attend the International Congress on Rheology in Monterey. The deadline for applications is 29 February 2008. Details of the Travel Grant program, eligibility requirements, and a description of the application process are on the web at www.rheology.org/sor/annual_meeting/2008Aug/student.htm.
Malvern’s rheological instruments have the unique ability to directly characterize material properties over 13 decades of shear rate. This means that physical material parameters can be measured, as well as their impact on process operation and end-use function.

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Suspension Rheology

Jan Mewis
Department of Chemical Engineering
K. U. Leuven Belgium

Norman Wagner
Department of Chemical Engineering
University of Delaware USA

The course is designed to be an introduction to the rheology of colloidal dispersions with emphasis on practical measurement and interpretation of rheological measurements on colloidal dispersions. The object is to provide the participants with:

• Qualitative understanding of the various phenomena that contribute to the rheology of suspensions;
• Scaling relations and quantitative laws to predict the basic rheology of such systems;
• Strategies to measure, characterize and design suspensions with well defined processing or application properties.

This course is of interest to students and practitioners of colloid rheology in industry as well as academia. A basic understanding of physical chemistry is necessary with some familiarity with colloidal science and basic rheology helpful but not required.

The course is structured so as to build systematically upon the fundamental understanding of how various properties of colloids and their interactions lead to the observed rheological behavior. This starts with systems where only purely hydrodynamic effects are present (i.e. suspensions with non-colloidal particles). Next, colloidal particles are introduced; with Brownian motion but without any particle interaction force. After that, systems with additionally repulse interparticle forces are dealt with: i.e. colloidal stable systems. Finally, attractive forces are added which can lead to flocculated suspensions and colloidal gels. The methods of rheological measurement and execution are discussed, treating the special difficulties that arise in the case of suspensions. Case studies will be analyzed to illustrate the basic concepts of the course. Special advanced topics are to be included depending on the interest of the students.

Surfactant Rheology

Self-Assembly and Microstructure Dynamics

Patrick T. Spicer
The Procter & Gamble Company
West Chester, OH 45069, USA

Srinivasa R. Raghavan
Dept. of Chemical & Biomolecular Engineering
University of Maryland, College Park USA

Although primarily known as modifiers of aqueous interfacial tension, surfactants exhibit a rich array of rheological behaviors as a result of their complex phase behavior. Consumer products are an example of the commercial use of surfactants for their cleaning and surface-treatment properties but also to modify liquid rheology. Additional surfactant research areas include drug delivery, nanoparticle synthesis by templating, and biophysical studies of cell transport.

This course will cover aqueous surfactant system rheology and its relationship with the numerous equilibrium phases formed. However, it also addresses the kinetic processes that are equally important to biological and industrial applications. The course theme is the theoretical and practical microstructure of different systems, their characterization, and their relationship with the resultant system rheology. The material is quantitative but highly visual, reflecting the topic's beauty via numerous illustrative movies and applications. Examples are drawn from applications in consumer products, pharmaceuticals, and petrochemicals.

The surfactant rheology course will enable industrial researchers, graduate students, and faculty members to more readily apply and understand surfactant rheological variations at high and low concentrations and will connect disparate areas of research that typically do not overlap.

More information is available on the web at www.rheology.org/ICR2008/ShortCourse/ShortCourse.htm
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Misuse of the Term *Pressure* in Rheology

John M. Dealy  
Department of Chemical Engineering  
McGill University

Abstract

The symbol $P$ is widely used to indicate an isotropic contribution to the total stress in describing the flow of non-Newtonian fluids, and whether explicitly stated or not, it is implied that the quantity referred to is the “pressure.” However, in most non-Newtonian fluids with structural or flow-induced anisotropy, there is no uniquely defined isotropic contribution to the total stress tensor. In experiments intended to show the effect of “pressure” on rheological properties, the quantity measured is, in fact, one component of the stress tensor and should be properly identified as such. Failure to recognize this fact can lead to error in the reporting of the data intended to show the effect of “pressure” on rheological properties. A meaningful variable for comparing data from different types of instrument is the mean compressive stress, which is the negative of the mean normal stress, but this quantity is not equal to the pressure that is measured, and its relationship to any measured pressure varies from one flow geometry to another.

Introduction

We are so accustomed to using the term “pressure” in thermodynamics and classical fluid mechanics that we continue to use it in situations in which its meaning is indeterminate. In particular, when dealing with flows in which deformation leads to anisotropy of the normal stresses, “pressure” has no unique definition. Thus, when we introduce a scalar to represent a contribution to the total stress, we introduce ambiguity into our equations. The universal failure to recognize this ambiguity results in ambiguity in reporting data said to indicate the effect of “pressure” on rheological properties.

We begin by noting the conditions under which it is acceptable to talk about the pressure $P$. For a fluid that has been at rest for a long time, *i.e.* at equilibrium, the stress is isotropic, which means that the normal stresses are the same in three orthogonal directions. Using the usual sign convention that compressive stresses are negative, since pressure is defined as a positive quantity, one can write:

$$
\sigma_{11} = \sigma_{22} = \sigma_{33} = -P
$$

Here $\sigma_i$ is a typical component of the total stress tensor. Devices for detecting pressure actually measure a particular normal stress component, and this can be said to be the pressure only if the stress is isotropic at the point of measurement. As we will see, except for the special case of a Newtonian fluid in simple shear flow, this is never the case in a flowing fluid. Most of this article deals with simple shear flow, and we will use the standard reference frame in which $x_i$ is the direction of flow, $x_j$ is the direction of the velocity gradient, and $x_k$ is the neutral direction. This is illustrated in Fig. 1.

Pressure plays a central role in thermodynamics as a state variable in equations of state. However, liquids, including molten polymers, are often assumed to be incompressible, in which case pressure becomes a strictly mechanical variable with no thermodynamic significance. While this assumption is convenient in solving fluid mechanics problems, it has the obviously unphysical implication that pressure has no effect on any physical property of the fluid. For example, if the density is unaffected by pressure, then the free volume is also unaffected, which implies that pressure has no effect on rheological properties.

For a viscoelastic fluid, if a deformation is sufficiently slow or small, the fluid is very close to its equilibrium state, the normal stress differences are zero, and it is appropriate to use pressure as a state variable. In other words, one can speak of the effect of pressure on linear viscoelastic properties such as the zero-shear viscosity and the storage and loss moduli. When the deformation is neither very slow nor very small, however, it is not in equilibrium, and classical thermodynamics is no longer strictly valid. Moreover, the normal stresses are not equal to each other, and there is no uniquely-defined scalar field that replaces pressure as a state variable.

A rheological constitutive equation for an incompressible fluid only specifies the stress to within an arbitrary isotropic component [1,2]. While this component is often given the symbol $P$ and called “pressure”, this is an unwise practice that leads to incorrect interpretations of experimental data. In order to avoid misunderstandings resulting from the use of the symbol $P$, we will call the as yet undefined isotropic contribution to the total stress $\pi$, which we
will consider, like the stress tensor, to be negative when the system is under compression. Thus, a rheological constitutive equation gives the “viscous” or “extra” stress tensor $\tau_{ij}$ as a function of the deformation field:

$$\sigma_{ij} = \tau_{ij} + \pi \delta_{ij} \quad (2)$$

where $\delta_{ij}$ is the kronecker delta. It is important to note that since two new quantities $\tau_{ij}$ and $\pi$ are introduced in Eq. 2, it does not define either one of them. For given flow kinematics, if a constitutive equation giving the components $\tau_{ij}(t)$ for a given strain history is assumed, then the components of the extra stress can be calculated. If the components of the total stress tensor are then measured, the value of $\pi$ at every point in the flow field can also be calculated. Thus, the expression for calculating $\pi$, given experimental values for the total stress components, depends on the choice of constitutive equation and the kinematics of the deformation. In the absence of a constitutive equation and a specified strain history, the scalar field $\pi$ is indeterminate. Furthermore, there are very few flow fields in which all the components of the total stress tensor can be measured, so practically speaking, $\pi$ is always indeterminate. And even if it could be calculated at each point in the flow, it has no known fundamental significance.

A constitutive equation may be written in such a way that the trace of the extra stress becomes zero when the fluid is at its rest state so that $\pi = -P$ [3]. But this does not imbue $\pi$ with any unique meaning when the fluid is subjected to a large, rapid deformation, and one is not at liberty to prescribe a priori that the trace of the extra stress be zero for any deformation.

**Normal Stresses in a Newtonian Fluid**

The simplest constitutive equation for a fluid is the incompressible Newtonian fluid model in which:

$$\tau_{ij} = \eta \dot{\gamma}_{ij} \quad (3)$$

where $\eta$ is the viscosity and $\dot{\gamma}_{ij}$ is a typical component of the rate-of-deformation tensor. The viscosity depends on temperature, pressure and composition but not on the deformation. Incompressibility can be prescribed in terms of either the rate of deformation tensor or the velocity vector $\vec{v}$:

$$\text{tr}(\dot{\gamma}) = 2 \nabla \cdot \vec{v} = 0 \quad (4)$$

Inserting (3) into (2), taking the trace, and making use of (4), we obtain:

$$\pi = \frac{1}{3} \text{tr}(\sigma_{ij}) \quad (Newtonian fluid) \quad (5)$$

But this is the definition of the mean normal stress. Thus, in an incompressible Newtonian fluid, $\pi$ is identical to the mean normal stress.

$$\pi = \sigma_{n} \quad (Newtonian incompressible fluid) \quad (6)$$

For the special case of a Newtonian fluid in simple shear flow, the diagonal components of the rate of deformation tensor are all zero. Thus, from Eqs 2 and 3, the normal stresses are all equal to each other and to $\pi$. In other words, in an incompressible Newtonian fluid in simple shear, the stress is isotropic, and pressure has the same meaning that it has in a fluid at rest.

$$\pi = \sigma_{11} = \sigma_{22} = \sigma_{33} = -P \quad (Newtonian fluid in simple shear) \quad (7)$$

In the fluid mechanics of Newtonian fluids, one can define the negative of the mean normal stress as “pressure.” However, except in simple shear flow, the normal stresses in a Newtonian fluid are not all equal, and the mean normal stress has no fundamental mechanical or thermodynamic significance. In other words, there is no known mechanism by which the properties of a fluid element react to this particular scalar field. Nevertheless, it is a well defined quantity, and in theory it can be measured, although it is rarely possible to measure all three normal stresses at every point within a material while it is being deformed. Thus, if one desired to measure the effect of compressive stresses on a property, the only
obvious choice of independent variable is the mean normal stress.

Flow of Viscoelastic Fluids

In a large, rapid deformation of a viscoelastic fluid, the stress is not isotropic, and the quantity \( \pi \) is not directly related to the mean normal stress or any other function of the normal stresses. Thus it is not justified to use the word “pressure” in describing the state of a viscoelastic fluid that is not in or very close to its equilibrium state. And while a Newtonian fluid is at equilibrium as long as it is at rest, a viscoelastic fluid must have been at rest for time longer than its longest relaxation time to be “at rest”. Total normal stresses of themselves have no rheological significance in an incompressible fluid, and it is only normal stress differences that are meaningful. The quantities actually measured are total or gauge normal stresses, but either a second total normal stress is also measured, or there is a free surface exposed to low-viscosity medium at a known pressure. For a flowing viscoelastic fluid there is no well-defined “pressure” that can be defined or measured.

There is an isotropic contribution to an extra stress that is used in dumbbell models of polymer solutions [2]. This term is proportional to \( kT \) and represents the contribution of the beads of the dumbbells to the stress. It has no effect on rheologically meaningful quantities but may be carried along in order that the extra stress will vanish in a solution that has been kept at rest and at a constant temperature for an indefinite period of time [3].

It is demonstrated below that in any viscometric flow, i.e., one that is, from the point view of a fluid element, indistinguishable from simple shear, the absolute magnitude of the mean normal stress in a polymeric fluid is always different from the environmental pressure to which any free surface of the sample is exposed. This is because the first normal stress differences are not zero except in the limit of very slow or very small deformations, when linear viscoelasticity is manifested. In simple polymeric liquids \( N_1 \) is normally positive, and \( N_2 \) is negative but considerably smaller than \( N_1 \), but this is not the case in systems such as stiff molecules that form liquid crystals and certain suspensions, when \( N_1 \) can be negative.

The remainder of this article deals exclusively with shear flows, but we note here that in uniaxial extension, where the surfaces of the sample are exposed to an environment at an ambient pressure \( P_a \), the mean normal (tensile) stress is given by:

\[
\sigma_m = \frac{1}{3} (\sigma_r - 2P_a)
\]

where \( \sigma_r \) is the tensile stress in the sample.

Flow in Tubes and Slits

For pressure-driven flow, starting from either Cauchy’s equation or a simple force balance in the flow \( (x_1) \) direction, one can derive a relationship between the gradient in the normal stress in this direction \( \sigma_{11} \) and the shear stress at the wall. But what is actually indicated by a pressure transducer mounted flush with the wall of the flow channel is -\( \sigma_{22} \), the normal stress in the direction of velocity gradient, evaluated at the wall. If the flow is fully developed, and if viscous heating and the effect of pressure on viscosity and normal stress differences are neglected, then the normal stress differences are independent of the axial coordinate \( x_1 \), and the gradient in the axial normal stress equals the gradient in the wall normal stress. Thus, it is possible to determine the viscosity without reference to an undefined isotropic contribution to the stress. And if the normal stress differences are known for the fluid of interest as functions of shear rate, the other normal stresses and the mean normal stress can be calculated.

As noted above while the mean normal stress has no known theoretical significance, it is at least a well-defined scalar field describing the level of tensile stress.

If a wall pressure sensor is not mounted flush with the wall but communicates with it by means of a small hole, the measurement is subject to pressure-hole error [4]. But if two or more identical pressure holes are used at various axial locations, the pressure-hole error, also called the hole-pressure, will be the same for each measurement and will cancel out when differences are calculated.

The Effect of “Pressure” on Rheological Properties

Failure to understand the issues raised above introduces an error in the comparison of data from different instruments intended to reveal the effect of “pressure” on rheological properties. Reports of “the effect of pressure on viscosity” have been based on the use of capillary, slit, concentric cylinder and sliding plate rheometers. Much of the work in this area has been cited by Koran and Dealy [5] and by
Cardinaels et al. [6]. What measure of the state of compressive stress in the fluid should be used to compare data obtained using various techniques? As we have seen, it is not appropriate to speak of pressure, and the only other well-defined scalar field that provides some measure of the state of compressive stress is the mean normal stress. We will now analyze several rheometrical flows in terms of the relationship between the normal stress that is measured (and incorrectly called the pressure of the sample) and the mean normal stress. For purposes of this demonstration we will assume that the first normal stress difference of the fluid is positive and is known as a function of shear rate. We will further assume that the second normal stress difference is $-aN_1$, where $a$ is approximately 0.2 [Ref. 7, pp 367, 368]. At the same time, it is noted once again that there are systems in which the normal stress differences do not behave like this.

In slit flow, the output of a pressure transducer mounted flush with the wall of the flow channel is the negative of the total wall normal stress, which is $-\sigma_{22}$. Since the normal stresses decrease along the flow, the quantity called pressure is the average of the measured values, which we will call the measured pressure $P_M$. We can relate the other normal stresses to this by means of the measurable normal stress differences as follows:

$$\sigma_{11} = \sigma_{22} + N_1 = -P_M + N_1$$  \hfill (9)

$$\sigma_{33} = \sigma_{22} + aN_1 = -P_M + aN_1$$  \hfill (10)

Thus, the mean normal stress is:

$$\sigma_m = \frac{1}{3} \left[ (P_M + N_1) - P_M + (P_M + aN_1) \right] = -P_M + \left[ (1 + a) / 3 \right] N_1$$  \hfill (11)

The mean normal stress is negative, because the sample is under compression, so for convenience we define the mean compressive stress $\sigma_c$ as $-\sigma_m$. Thus,

$$\sigma_c = P_M - \left[ (1 + a) / 3 \right] N_1$$  \hfill (12)

Thus, the mean compressive stress is less than the measured pressure.

There are several types of high-pressure Couette rheometer, and the analysis depends on how the system is pressurized and where the pressure is measured. A more straightforward case is cone-plate flow, where the only surface of the sample that is exposed to the pressurized environment is the outer rim. If the sample is trimmed flush with the outer edges of the cone and plate, the measured pressure $P_M$ is $-\sigma_{rr}$. We now express the mean normal stress in terms of this measured quantity.

$$\sigma_{\theta\theta} = \sigma_{rr} + N_2 = \sigma_{rr} - aN_1 = -P_M - aN_1$$  \hfill (13)

$$\sigma_{\phi\phi} = \sigma_{\theta\theta} + N_1 = (\sigma_{rr} - aN_1) + N_1 = \left[ -P_M + (1 - a)N_1 \right]$$  \hfill (14)

$$\sigma_c = -\sigma_m = P_M - \frac{1}{3} (1 - 2a)N_1$$  \hfill (15)

where $\sigma_{rr}$ is the normal stress in the radial (neutral) direction, $\sigma_{\theta\theta}$ is the normal stress in the angular (direction of motion) direction, and $\sigma_{\phi\phi}$ is the normal stress in the azimuthal (velocity gradient) direction. Once again, the mean compressive stress is less than the measured pressure.

In a sliding plate rheometer the imposed pressure $P_M$ is approximately $-\sigma_{11}$, and this is related to the mean compressive stress as follows:

$$\sigma_c = P_M + \frac{1}{3} (2 - a)N_1$$  \hfill (16)

In this case, the mean compressive stress is greater than the measured pressure.

The usual practice in reporting the effect of “pressure” on viscosity is to plot viscosity versus $P_M$, but we see from the above analyses that to compare data from different instruments, it is $\sigma_c$ that should be used as the independent variable. Another way of looking at this is that if data from two instruments are compared by plotting viscosity versus $P_M$, each set of data should be shifted on the $P_M$ axis by the amount indicated by the above equations. Unfortunately, this is not feasible at the present time, as even if $N_1$ and $N_2$ at ambient conditions have been measured for the polymer of interest, nothing is known about the effect of $\sigma_c$ on the normal stress differences.

(continues page 26)
Montgomery T. Shaw Receives SOR Distinguished Service Award

by Andy Kraynik, SOR Past President

Montgomery T. Shaw received the Distinguished Service Award of The Society of Rheology at the 79th Annual Meeting in Salt Lake City. The ceremony may have come as a surprise to Monty, but not to any member of the Society in the past three decades. He is the eighth recipient of this honor, which is awarded infrequently at the discretion of the Executive Committee for exceptional service to the Society.

Monty has served the Society in elected office as Secretary (1977-1981), Member-at-Large (1983-1985), and Treasurer (since 1997). He has also served on the Bingham Award Committee (1989-1991), the Nominating Committee (1991), and as Technical Program Chair for the 62nd Annual Meeting in Santa Fe (1990). An appointment to the position of Associate Editor for Finance (1995-1997) prepared him for his current office, where he has overseen substantial growth in the financial resources and financial responsibilities of the Society. Monty’s tenure as Treasurer followed that of Ed Collins, who had received the second Distinguished Service Award in 1986 and served as Treasurer for a total of twenty-six years. Monty may not break Ed’s record, but then again no one has overheard him to say that he won’t try. It’s hard to imagine a time when Monty won’t be serving the Society in some capacity – the position of Society Historian may not exist, but we all know the perfect candidate!

Monty received BChE and MS degrees in chemical engineering from Cornell University in 1966, and a PhD in chemistry (1970) from Princeton University, where he studied under the late Professor A.V. Tobolsky. He then worked in the R&D department of the Union Carbide Corporation in Bound Brook, NJ until 1977, when he joined the faculty of Chemical Engineering at the University of Connecticut. He now serves as Interim Head of the new Chemical, Materials and Biomolecular Engineering Department at UConn. Monty is associated with the nearby Institute of Materials Science where he conducts research on polymer solution and blend thermodynamics, polymer rheology and processing, and polymer aging. He has received numerous rewards for his research and scholarship.

Monty is an avid outdoorsman. His wife Maripaz is well known to many members of the Society and his son Steven is an Associate Professor in the Electrical and Computer Engineering Department at Montana State University in Bozeman.
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The opening reception in Salt Lake City drew an enthusiastic crowd.

Brady is well known for his contributions in suspension rheology, particularly as the originator, with G. Bossis, of the simulation technique known as Stokesian dynamics. At the Bingham Lecture Brady was introduced by his PhD thesis advisor, Andreas Acrivos, currently at the Levich Institute for Physicochemical Hydrodynamics at the City University of New York. In addition to microrheology (asking, provocatively, is it rheology?), Brady took time to make a pitch for additional scientific credit to be given to the early 20th century researcher William Sutherland. The well-known Stokes-Einstein relationship is usually credited to work published by Einstein in 1905, but appearing the same year, and earlier, was the same relationship in a paper by William Sutherland. Thus, the Stokes-Einstein-Sutherland relationship is born.

The technical sessions opened with a plenary presentation by Fabian Waleffe from the Department of Mathematics at the University of Wisconsin, Madison.

(continues page 18)
Are you compounding expensive materials such as nano-composites, biopolymers or pharmaceuticals? Do you simultaneously want to record rheological properties to document structural changes? Then we have the answer. The Thermo Scientific Micro-Compounder HAAKE MiniLab can mix a sample and analyze its rheological properties with as little as 5 g.

Main features:
• Co- and counter rotating twin screws
• Integrated viscosity measurement
• Automatic bypass operation for circulation/extrusion
• Pneumatic feeding
• Manual or computer control
• Easy to clean due to exit in split barrel

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Bingham medalists present in Salt Lake City included: Morton Denn, Henning Winter, John Brady (2007 medalist), Gary Leal, Andreas Acrivos, Gerry Fuller, Ronald Larson, William Russel, John Dealy, and Chris Macosko.

Waleffe spoke on “Exact coherent states: controlling turbulence and transition.” The Wednesday plenary presentation was given by Jennifer Lewis from the Department Materials Science and Engineering at the University of Illinois, Urbana. Lewis’ presentation on “Novel ink designs for direct writing in three dimensions” showed how precise control of flows on nano- and micro-scales can lead to important applications in the printing industry.

The social program at the SOR meeting was jam-packed, as usual. The Sunday reception, hosted by TA Instruments, took place at the Alpine Ballroom of Hilton and welcomed all to the meeting. On Tuesday evening the awards reception, sponsored by Xpansion Instruments, served as a gathering place before the Bingham banquet at which Brady was roasted by no fewer than four presenters. Andy Acrivos (with some prompting from the audience), Jon Higdon (fellow Churchill Scholar at Cambridge with Brady), and former Brady students Roger Bonnecaze and Jeff Morris covered every aspect of Brady’s persona, personal and professional, injecting humor while making clear their great respect for the 2007 Bingham medalist.

For many attendees the poster session is a most enjoyable part of the meeting, as there is opportunity for casual interaction within a stimulating scientific environment. In Salt Lake the refreshments at the poster session were sponsored by Anton-Paar USA. For student attendees, the Student Poster Competition is much anticipated, and the recipient of that prize in 2007 was Mukund Vasudevan from Washington University in St. Louis (see article page 21). Conference bags were sponsored by Malvern Instruments.

As the Salt Lake meeting drew to a close we were reminded that our next meeting will be the International Congress on Rheology, taking place in 2008 in Monterey, California USA in less than a year. Details on ICR2008 may be found in this Bulletin (page 4).
Application for Membership in The Society of Rheology

Any student, scientist or engineer with an interest in the deformation or flow of matter is invited to join The Society of Rheology. Members receive the Rheology Bulletin, the Journal of Rheology and Physics Today. There are no academic or geographic requirements for membership. Complete and send a copy of this application form to the address below.

I wish to apply for membership in The Society of Rheology dating from January ____________ (year)

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| affiliation:        | academia | industry | government | (check most appropriate) |
| regular member ($40) |           |           |            | (include copy of student ID) |
| student member ($25) |           |           |            |                             |

| credit card:        | AMEX | MasterCard | Visa | exp. date: |
| card number:        |      |            |      |            |

signature: __________________________ date: __________________________

Please enclose remittance in US dollars drawn on a US bank payable to “The Society of Rheology” and mail to Janis Bennett at AIP, Suite 1NO1, 2 Huntington Quadrangle, Melville, NY 11747-4502, 516-576-2403, 516-576-2223 (fax). A member subscription to the Journal of Rheology is only for your personal use. By your signature below, you agree not to loan or give any issues of this journal to a library or other lending institution without written permission from The Society of Rheology.

signature (required): __________________________ date: __________________________
SoR Student-Member Travel Grants Available for ICR2008

Student members of The Society of Rheology are invited to apply for travel grants to attend the International Congress on Rheology in Monterey. The deadline for applications is 29 February 2008. Details of the program, eligibility requirements, and a description of the application process are on the web at www.rheology.org/sor/annual_meeting/2008Aug/student.htm.

New Award from the Society of Rheology?

By Lynn Walker, ExCom Member-at-Large 2005-2007

The Society of Rheology currently presents the following awards: Bingham medal (annually), Poster Presentation Award (annually), Publication Award (annually) and the Service Award (intermittent). During the business meeting held at the 2007 Meeting in Salt Lake City, a presentation was made about the need for new awards and possible formats for new awards.

The pros and cons of giving additional awards were first discussed. There seemed to be a general agreement from the audience that the Society should consider offering more awards. The Society membership is large enough to support more awards without diluting the meaning of the current awards. Additional awards will provide publicity for the Society and recognition of its members.

Several different options for new awards were presented and more were offered during the discussion. The possible awards suggested were: an early career award (targeting a researcher under the age of 35 or 40), a best thesis award, a graduate research presentation award, and an award for innovation in industrial rheology. During the discussion, suggestions were made regarding the pragmatics of an award process, pros and cons of the different options, concerns over conflict with existing awards (specifically the award given at the poster session), and comparisons that could be made to awards given by other societies. A vote was not called on this issue, instead it was decided that the Executive Committee should make decisions and present a formal proposal at a future date. An unofficial poll was taken by show of hands for the different awards. There was considerable support for the early career award. Support for a thesis award or some type of award for industrial innovation was also shown, but with less enthusiasm.

The topic will be discussed at the March meeting of the Executive Committee. At that time, it is likely that the ExCom will decide on the best options for new awards. Members of the Society with comments, ideas or suggestions should contact any member of the Executive Committee prior to March with input.

SOR Always Needs Volunteers: Consider Getting Involved

Members of The Society of Rheology who are interested in getting more involved with Society affairs are encouraged to contact a member of the Executive Committee to express interest. Standing committees on Membership and Education are reconstituted with every election. Volunteers are also needed from time to time for ad hoc assignments that benefit the Society, such as serving as a representative of the SOR to external committees. Contact current committee members for more information on the duties that these positions involve. See page 3 for a list of committee members and Society officers and representatives.
Contribution from Washington University St. Louis Receives SLC Student Poster Award

Mukund Vasudevan received the SOR Student Poster Presentation Award at the 79th Meeting of The Society of Rheology in Salt Lake City in October 2007 for his poster entitled, “Self-similar shear thickening behavior in CTAB/NaSal surfactant solutions.” Vasudevan is a student at Washington University in St. Louis, in the Department of Energy, Environmental and Chemical Engineering. Co-authors on the research were Amy Shen, Bamin Khomami, and Radhakrishna Sureshkumar.

Vasudevan’s research is concerned with the rheological properties of wormlike surfactant solutions that undergo a phase transition from a solution phase to a gel-like phase upon increasing the shear rate above a critical value. In their study, Vasudevan and coworkers investigated the effect of salt concentration on rheological behavior in the shear-thickening regime.

¡Caminaron sobre el agua! (Let’s walk on water!)

The shear-thickening properties of cornstarch/water mixtures are well known to rheologists, and many school outreach programs use this system for great “wow!” effect. But have you ever wondered if you could run across a pool of it?

The question has been addressed definitively by the Spanish television program El Hormiguero (Spanish for “The Anthill”). El Hormiguero uses humor to address a wide variety of topics, including science. On 9 October 2006, host and producer Pablo Motos and companion “Flipy the scientist” ran repeatedly across a pool of cornstarch/water that appears to be about 1.5 meters wide, 3 meters long and 1 meter deep. A cement truck had been called in to effect the mixture. A video of their antics is available on the show’s website (www.cuatro.com/multimedia/video.html?xref=20061009ctoultnot_3.Ves) and is also posted on YouTube.com (search for “cornstarch water pool” or “non-Newtonian”).

The cornstarch/water system has come to be known as oobleck, and the standard recipe for oobleck is approximately 1 part water to 1.5–2 parts cornstarch. The word ooblech, besides invoking a common reaction to the fluid, refers to a Dr. Seuss children’s book, “Bartholomew and the Oobleck,” which features a green goo that gums up everything it touches.

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Bingham Nominations Sought

Nominations are invited for the 2008 Bingham Award, which will be presented at the XVth International Congress on Rheology in Monterey. The Bingham Award is presented annually to an individual who is a resident of North America or a member of the Society who has made outstanding contributions to the field of rheology. The deadline for nominations is 15 January 2008. Additional information and revised guidelines for preparing a nomination can be found on the SOR website at www.rheology.org/sor/awards/Bingham/nom2008.htm.

Minutes of the ExCom Meeting

Sunday 7 October 2007
Salt Lake City, Utah USA

Attending: Andy Kraynik, Monty Shaw, Tim Lodge, Joao Maia, Albert Co, Bob Prud’homme, Dan Klingenberg, Skip Rochefort, Marie-Claude Heuzey, Lynn Walker, John Brady, Janis Bennett, Susan Muller, Gerry Fuller, Norm Wagner, Mike Solomon, Jaye Magda, Gary Leal, Bob Powell, Pat Mather, Faith Morrison.

President Kraynik called the meeting to order at 8:30 am in the Granite Boardroom of the Hilton Salt Lake City Center. Past-President and Acting Secretary Susan Muller read the minutes of the last Executive Committee meeting. The minutes were approved after correcting a typo in the first two words.

Monty Shaw provided a financial report. The Journal of Rheology is making a profit, primarily due to online subscriptions. Advertising revenue for the Rheology Bulletin has increased since last year. The financial position of the Society is sound. Janis Bennett proposed that if a member pays for an online subscription during the fall renewal cycle (typically September), their online subscription begins as soon as payment is received and their IP is set up and continues through the following December. This motion was made and passed. Monty Shaw discussed the accounting difficulties associated with meetings; frequently meeting accounts start two to three years before the meeting with payment of a deposit to the hotel, and accounts are not completely cleaned up and closed until the March after the meeting. Thus meetings do not fit easily into the year-to-year accounting that we report for all other Society activities.

John Brady gave the Journal of Rheology Editor’s Report. Submissions reflect a slight diminution in time. This may correct itself by year’s end. Brady presented submissions by country of origin for the past year. South Korea had 100% acceptance rate, followed by 80% from Belgium. Overall acceptance rates for manuscripts are 45%, days from receipt to first decision are 87, days from receipt to final decision are approximately 112.

Skip Rochefort reported as the SOR representative on the AIP Liaison Committee for Under-Represented Minorities. This committee is charged with coordinating diversity initiatives among AIP member societies and encouraging participation by under-represented minorities. Skip discussed the possibility of the SOR supporting K-12 outreach activities and a travel grant for undergraduates in under-represented groups who are working in rheology to attend the annual meeting.

Jaye Magda reported on the SLC meeting. The reservation for the Monday night reception at the Museum of Utah Art & History was cancelled by the museum due to construction delays. Registration is currently 301 registrants; additional on-site registrations are anticipated. Approximately 40 students are taking one or the other short course. There are 14 exhibitors. Exhibitors and sponsors are providing a significant amount of support for the meeting.

Lynn Walker led a discussion of a new Society of Rheology award, directed at either graduate student or an early career award (under 35 or 40). Lynn will present the advantages and disadvantages of such awards for discussion with the membership at the Business Meeting.

Gerry Fuller led a discussion of the ICR, which will serve as the SOR Annual Meeting for 2008. Gerry cautioned that Monterey is an expensive venue, and that attendees should be cautioned about the high cost of lodging. The SOR has negotiated a very good rate for Monterey; while lower cost options are available some distance away, parking in Monterey is ex-
Treasurer’s Report

To the Membership:

Those of you who attended the Society’s Annual Business Meeting in Salt Lake may recall that there were some 2008 budgeting uncertainties that were dependent on the financial prognosis for the International Congress. The Membership consequently approved a budget that allowed for minor changes to appear in the final version published in January.

According to the latest reports on abstract submissions, the process was extremely difficult and expensive. Gary Leal discussed the Technical Program and important deadlines for the conference proceedings.

Andy Kraynik discussed officer succession. Andy also provided a brief update on the 2010 Santa Fe meeting. Pat Mather described preparations for the 2011 Cleveland meeting. Pat reported that membership in the SOR is stable at approximately 1500 members. Andy mentioned that since the International Congress will be held in Europe in 2012, the next SOR meeting after Cleveland will be a winter meeting in 2013; proposals for that meeting will be solicited at the Business Meeting.

Albert Co presented voting statistics (percentage of votes by country) and submission statistics for the SLC meeting. A motion was made to no longer offer overhead projection as a visual aid option on the submission website for future meetings. The motion passed.

Janis Bennet reported that Fred Dylla is the new Executive Director and CEO of AIP, replacing Marc Brodsky. AIP’s membership director, Lorrie Carlin, directed Janis to mention ConferenceDirect, who works with other AIP member societies to negotiate meeting contracts. The Executive Committee expressed skepticism but will look into this further.

Mike Solomon reported for the Education Committee. Morrison and Giacomin had 18 students in their “Beginning Rheology” course; Squires, Anna, Doyle, and Breedveld had 25 in “Microfluidics for Rheologists.” Short courses at the 2008 ICR meeting in Monterey will be a 2-day “Suspension Rheology” course by Mewis and Wagner, and a 1-day “Surfactant Rheology – Self-Assembly and Microstructure Dynamics” course by Spicer and Raghavan.

Bob Prud’homme volunteered to review honoraria and prize amounts on the traditional 4-year cycle at the Spring 2008 Executive Committee meeting.

Faith Morrison has turned over all issues related to Rheology Bulletin Advertising to AIP. This has worked out very well. Morrison discussed succession issues for the Bulletin Editor once she becomes SOR Vice President. She discussed difficulties in putting older versions of the Rheology Bulletin on the web; she and Albert Co are working to resolve these issues.

The meeting entered Executive Session at 4:24 pm. The meeting was adjourned at 5:00 pm.

Minutes of the Business Meeting

Tuesday, October 9, 2007
Salt Lake City, Utah

Andy Kraynik called the meeting to order at 6:15 p.m. in the Alpine East room of the Hilton Salt Lake City Center. The minutes of the previous Business Meeting in Portland, Maine were read and approved without addition or correction.

Each officer report and each committee report presented at the Executive Committee meeting (see above) was presented and accepted. A motion was entertained to keep the Bingham Award nomination deadline in mid-January rather than advancing it to mid-December in conjunction with the advanced annual meeting date (August ICR). The membership voted resoundingly to keep the deadline in mid-January. Lynn Walker led a discussion about new awards. Majority support was expressed by the membership for considering the creation of (1) a thesis award, (2) an early career award, and (3) an award for industrial and pragmatic application of rheology. John Dealy led a discussion about reducing the library subscription rate for the Journal of Rheology to lessen the growth rate of Society reserves. Andy Kraynik passed the gavel of the Society to incoming President Bob Prud’homme.

The meeting was adjourned at 6:55 p.m.

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tion, the financial situation for the ICR is now quite promising, so the 2008 Budget has been tightened up with a return to the usual breakeven position for an annual meeting. However, with a more liberal student-travel policy for the ICR, the anticipated disbursement for this line item has been increased. While the accounting for Salt Lake City has not been completed, the indications are that the final position for the meeting will be positive. Thus the financial picture for the Society remains very favorable as the end of 2007 approaches.

Respectfully submitted,
Montgomery T. Shaw, Treasurer

The Society of Rheology, Inc.
Balance Sheet

(all amounts, USD)

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| **Liabilities and Net Assets** |     |               |             |               |               |
| Liabilities             |             |               |             |               |               |
| Deferred revenue        | 0           | 129,339       | 0           | 132,396       | 155,969       |
| Total Liabilities       | 0           | 129,339       | 0           | 132,396       | 155,969       |

| Net Assets              |             |               |             |               |               |
| Publication reserve     | 450,000     | 450,000       | 450,000     | 450,000       | 450,000       |
| Student Travel Grant reserve | 10,000        | 10,000        | 10,000      | 10,000        | 10,000        |
| Annual Meeting reserve  | 300,000     | 200,000       | 300,000     | 200,000       | 100,000       |
| Operating reserve       | 100,000     | 100,000       | 100,000     | 100,000       | 100,000       |
| Unrestricted            | 425,184     | 306,416       | 282,447     | 176,513       | 189,698       |
| **Total Net Assets**    | 1,285,184   | 1,066,416     | 1,142,447   | 936,513       | 849,698       |

| Total liabilities and net assets | 1,285,184 | 1,195,755 | 1,142,447 | 1,068,909 | 1,005,667 |

Journal of Rheology
Receipts and Disbursements

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| **DISBURSEMENTS**       |             |                 |             |             |               |
| Ads                     | 7,000       | 11,047          | 6,553       | 9,500       | 7,199         |
| Reprints, Single Copy   | 1,900       | 2,203           | 1,195       | 5,400       | 1,647         |
| Paper, Printing         | 20,000      | 22,607          | 13,668      | 29,638      | 18,502        |
| SOR Editorial           | 41,000      | 44,489          | 27,100      | 42,000      | 39,534        |
| Production              | 30,000      | 36,335          | 21,010      | 55,000      | 29,841        |
| Fulfillment             | 6,425       | 5,987           | 3,871       | 6,625       | 6,364         |
| Distribution            | 20,100      | 17,797          | 12,796      | 20,833      | 18,724        |
| Electronic Publishing   | 35,000      | 33,058          | 22,654      | 43,000      | 33,570        |
| Miscellaneous           | 4,800       | 6,071           | 2,294       | 6,000       | 5,494         |
| **TOTAL DISBURSEMENTS** | 166,225     | 179,595         | 111,141     | 217,996     | 160,874       |
| Net                     | 91,975      | 103,748         | 137,773     | 44,604      | 106,080       |
The Society of Rheology
Receipts and Disbursements
(all amounts, USD)

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Pressure, continued from page 13

For the special case of very low shear rates, where it is \( \eta \) that is measured, the pressure is essentially isotropic, and it is appropriate to speak of the effect of pressure. Also, if \( P_m \) is much larger than \( N_c \), the uncertainty in using \( P_m \) in place of \( \sigma \) will probably be within the experimental uncertainty. For example, Park et al. [8] used several types of rheometer to study the effect of “pressure” on the viscosity of a styrenic polymer. Not only was the mean compressive stress unknown, but its relationship to the measured pressure varied from one rheometer to another. They estimated that the maximum value of the first normal stress difference, over the range of shear rates involved, at 12 MPa applied pressure \( (P_m) \) was 0.4 MPa, while that at 70 MPa was 1.3 MPa. Thus, the uncertainty in the mean compressive stress was 4% at most, which was within the range of experimental uncertainty.

Conclusions

In the deformation of a viscoelastic fluid, unless the deformation is either very small or very slow, it is inappropriate to use the term pressure to describe the state of the sample. If the kinematics of the deformation is specified and a constitutive equation is selected, then experimental values of the total stress components can be used to calculate the value of \( \pi \) at every point in the flow field, but it is not unique and has no fundamental significance. A well-defined scalar that describes the state of compressive stress in a polymeric liquid is the mean compressive stress \( \sigma \). Any pressure that is measured in the environment to which a surface of the sample is exposed is only one component of the total stress tensor, and its relation to \( \sigma \) depends on the material and varies from one type of flow to another. This can lead to uncertainty in reporting the results of measurements of the effect of compressive stress on the rheological properties of viscoelastic fluids. In reporting the results of such measurements, while the quantity actually measured is a pressure, the relationship of this quantity to the mean compressive stress in the sample depends on the kinematics of the flow. For example, in slit flow, the quantity measured by a pressure transducer mounted in the wall is \( -\sigma_{rr} \), and for cone-plate flow the imposed pressure is equal to \( -\sigma_{rr} \). A useful parameter for use in comparing data from different types of rheometer is the mean compressive stress, but to compute this from the measured pressure requires knowledge of the first and second normal stress differences as functions of shear rate and pressure.

Acknowledgement

Errors arising from the use of the term “pressure” in non-Newtonian fluid mechanics have troubled me for decades, but it was only when prodded by recent discussions with Prof. C. D. (Paul) Han of the University of Akron that I was inspired to write what I hope is a clear statement of the problem.

List of Symbols

\[
P \quad \text{Pressure}
\]
\[
P_m \quad \text{Measured pressure}
\]
\[
r \quad \text{Radial coordinate in cone-plate flow}
\]
\[
\hat{V} \quad \text{Velocity vector}
\]
\[
\gamma \quad \text{Rate of deformation tensor}
\]
\[
\gamma_{ij} \quad \text{Typical component of the rate of deformation tensor}
\]
\[
\delta_{ij} \quad \text{Kronecker delta} \ (\delta_{ij} = 1 \text{ when } i=j; \ \delta_{ij} = 0 \text{ when } i\neq j)
\]
\[
\eta \quad \text{Viscosity of a Newtonian fluid}
\]
\[
\theta \quad \text{Azimuthal coordinate in cone-plate flow}
\]
\[
\pi \quad \text{An isotropic contribution to the total stress} \ (\text{positive when compressive})
\]
\[
\sigma \quad \text{Stress tensor}
\]
\[
\sigma_c \quad \text{Mean compressive stress} = -\sigma_m
\]
\[
\sigma_n \quad \text{Mean normal stress} \ (\text{trace of } \sigma)
\]
\[
\sigma_{ij} \quad \text{Typical component of the total stress tensor}
\]
\[
\sigma_{ij}^N \quad \text{Component of the normal stress in the flow direction (simple shear)}
\]
\[
\sigma_{22} \quad \text{Component of normal stress in direction of velocity gradient (simple shear)}
\]
\[
\sigma_{33} \quad \text{Component of normal stress in the neutral direction (simple shear)}
\]
\[
\sigma_{00} \quad \text{Component of normal stress in the azimuthal direction (cone-plate flow)} = \sigma_{11}
\]
\[
\sigma_{00}^A \quad \text{Component of normal stress in angular direction (cone-plate flow)} = \sigma_{22}
\]
\[
\sigma_{rr} \quad \text{Component of normal stress in the radial direction (cone-plate flow)} = \sigma_{33}
\]
\[
\tau \quad \text{Typical component of the extra stress tensor}
\]
\[
\phi \quad \text{Angular coordinate in cone-plate flow (direction of rotation)}
\]

References


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See also:
www.rheology.org/sor/info/Other_Meetings.htm
www.rheology-esr.org/Meetings.php
www.appliedrheology.org/ (click on conferences)
CALENDAR OF RHEOLOGY CONFERENCES AND COURSES

2008

8-13 June 2008
University of Minnesota's Annual Rheological Measurements Short Course, Chris Macosko, Director, www.cems.umn.edu/rheology

15-19 June 2008

2-3 August 2008
SOR Short Course on Suspension Rheology, by Jan Mewis and Norman Wagner, Monterey, CA USA; option is available for participants to attend the first day of Suspension Rheology course on Saturday and the Surfactant Rheology course (below) on Sunday.

3 August 2008
SOR Short Course on Surfactant Rheology - Self-Assembly and Microstructure Dynamics, by Patrick T. Spicer and Srinivasa R. Raghavan, Monterey, CA USA

3-8 August 2008
XVth International Congress on Rheology and 80th Annual Meeting of The Society of Rheology, Monterey, CA USA, Gerry Fuller and Bob Powell, www.rheology.org/ICR2008/

24-30 August 2008

9-13 July 2008
The 13th International Congress of Biorheology and the 6th International Conference on Clinical Hemorheology, State College, Pennsylvania, USA, Herbert Lipowsky and Herbert Meiselman (www.outreach.psu.edu/programs/isbisch/; held every three years).

2009

Spring 2009
5th Annual European Rheology Conference AERC 2009, location TBA

15-18 June 2009
5th International Symposium on Food Rheology and Structure - ISFRS 2009, Peter Fischer, Zurich Switzerland (every 3 years; www.isfrs.ethz.ch)

Summer 2009
5th Pacific Rim Conference on Rheology, location tentatively Hokkaido, Japan, Hiroshi Watanabe (every 4 years)

17-18 October 2009
SOR Short Course on Rheology (topic TBA), Madison, WI USA

18-22 October 2009
81st Annual Meeting of The Society of Rheology, Madison, WI USA, Jeff Giacomin

2010

Spring 2010
6th Annual European Rheology Conference AERC 2010, location TBA

23-24 October 2010
SOR Short Course on Rheology (topic TBA), Santa Fe, NM USA

24-28 October 2010
82nd Annual Meeting of The Society of Rheology, Santa Fe, New Mexico USA, Andy Kraynik

2011

Spring 2011
7th Annual European Rheology Conference AERC 2011, location TBA

8-9 October 2011
SOR Short Course on Rheology (topic TBA), Cleveland, Ohio USA

(Meetings continues p27)